

# MODELING WATER CHEMISTRY CHANGES DURING THE DRINKING WATER TREATMENT PROCESS

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# Outline



- Need for Modeling
- Treatment Process
- Goals for Modeling
- Modeling Procedure
- Future Work/Improvements
- Questions

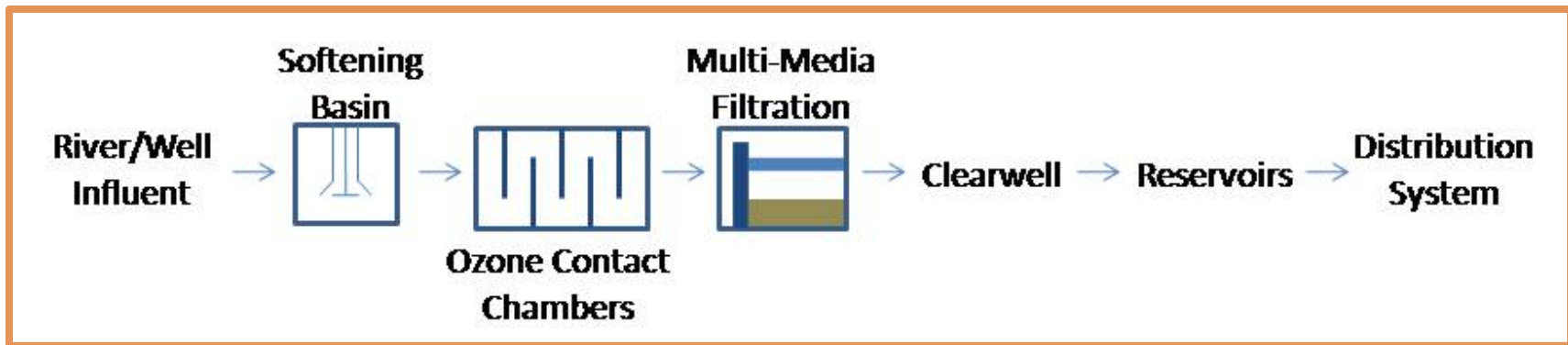
# Need for Modeling



- Different Source Waters
  - ▣ Mixing ratios between river and wells constantly change
  - ▣ Different water sources have different chemistry
  - ▣ Better understanding would improve:
    - Chemical use efficiency
    - Better treatment
    - Save money
- Not much published yet

# Treatment Process

## □ Moorhead Water Treatment Plant (MWTP)



- Influent Water Mixing
- Sedimentation and Softening
- Ozone Disinfection/Recarbonation
- Multi-media Filtration

# Goals for Modeling

- Three Processes:
  - ▣ Mixing
  - ▣ Softening
  - ▣ Recarbonation
- Mixing
  - ▣ Determine combined hardness and pH
- Softening
  - ▣ Hardness: 88 to 108 mg/L as  $\text{CaCO}_3$
  - ▣ pH: 10.5 to 11.5
- Recarbonation
  - ▣ Hardness: 88 to 108 mg/L as  $\text{CaCO}_3$
  - ▣ pH of 9.5 to 9.7

# Modeling Procedure



- Influent Water Chemistry

- Mixing

Simulation 1

- Softening

Simulation 2

- Recarbonation

Simulation 3

# Mixing Model

- Water Sources
  - ▣ Groundwater (GW)
    - Buffalo Aquifer
  - ▣ Surface Water
    - Red River



# Mixing Model

|   | Parameter/Constituent (unit)       | Red River | GW     |
|---|------------------------------------|-----------|--------|
| → | Temperature (°C)                   | 25.08     | 8.58   |
|   | pH(units)                          | 8.2       | 7.6    |
|   | Oxidation Reduction Potential (mV) | 47        | 96.5   |
|   | Alkalinity, Bicarbonate (mg/L)     | 190       | 330    |
|   | Alkalinity, Carbonate (mg/L)       | 2.6       | 1.3    |
|   | Alkalinity, Total (mg/L)           | 190       | 330    |
|   | Barium (µg/L)                      | 76.9      | 46.6   |
|   | Bromide (mg/L)                     | 0.0496    | 0.0744 |
| → | Calcium (mg/L)                     | 51        | 94.6   |
|   | Chloride (mg/L)                    | 13        | 14.9   |
|   | Iron (µg/L)                        | 851       | 1050   |
|   | Magnesium (mg/L)                   | 37.3      | 36.9   |
|   | Manganese (µg/L)                   | 70.4      | 120    |
|   | Phosphate, Total (mg/L)            | 0.424     | 0.272  |
|   | Potassium (mg/L)                   | 4.6       | 5      |
| → | Sodium (mg/L)                      | 0.5       | 62.5   |
|   | Strontium (µg/L)                   | 200       | 504    |
|   | Sulfate (mg/L)                     | 86.7      | 170    |
|   | Dissolved Oxygen (mg/L)            | 3.3       | 0.32   |



# Mixing Model

SOLUTION 1 Red River  
temp 25.08  
pH 8.2  
pe 0.7945  
redox pe  
units mg/l  
density 1  
Alkalinity 190 as HCO<sub>3</sub>  
Ba 0.0769  
Br 0.0496  
Ca 51  
Cl 13  
Fe 0.851  
Mg 37.3  
Mn 0.0704  
P 0.424  
K 4.6  
Na 0.5  
Sr 0.2  
S(6) 86.7  
O(0) 3.3  
-water 1 # kg

SOLUTION 2 Well 9  
temp 8.58  
pH 7.6  
pe 1.73  
redox pe  
units mg/l  
density 1  
Alkalinity 330 as HCO<sub>3</sub>  
Ba 0.0466  
Br 0.0744  
Ca 94.6  
Cl 14.9  
Fe 1.05  
Mg 36.9  
Mn 0.12  
P 0.272  
K 5  
Na 62.5  
Sr 0.504  
S(6) 170  
O(0) 0.32  
-water 1 # kg

MIX 1  
1 0.72  
2 0.28  
SAVE solution 3  
END

# Mixing Model

## Prior to Mixing

- Phreeqcl Speciation
  - ▣ Ionic Strength
    - Red River:  $8.262 \times 10^{-3}$
    - GW:  $1.410 \times 10^{-2}$
  - ▣ Hardness
    - Red River: 252.50 mg/L
    - GW: 344.40 mg/L
  - ▣ pH
    - Red River: 8.2
    - GW: 7.6

## After Mixing

- Phreeqcl Speciation
  - ▣ Ionic Strength
    - $9.892 \times 10^{-3}$
  - ▣ Hardness
    - 279.2 mg/L
  - ▣ pH
    - 7.8

Flows: River=2500 gpm and GW=995 gpm → 5 MGD

Mixing Ratio: 72% River to 28% GW

# Softening Model

□ Hardness is measured by amount of  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$

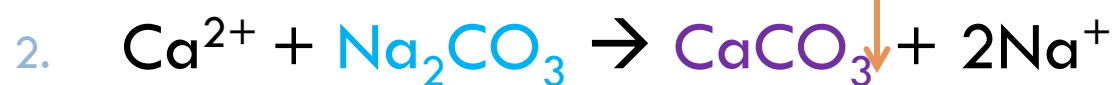
□ Hardness Causes:

□ Scale-pipes and fixtures

□ High soap consumption-no lathering

□ Hardness Removal:

□ lime [ $\text{Ca}(\text{OH})_2$ ] and soda ash [ $\text{Na}_2\text{CO}_3$ ]



□ precipitation of calcite [ $\text{CaCO}_3$ ] and brucite [ $\text{Mg}(\text{OH})_2$ ]

# Softening Model

## □ Input Code

USE solution 3

REACTION 1

Portlandite 1

$\text{Na}_2\text{CO}_3$  0.5

0.002 moles in 1 steps

EQUILIBRIUM\_PHASES 1

Brucite 0 0

Calcite 0 0

Portlandite 0 0

SAVE solution 4

END

## □ Phreeqc Results

□ Hardness: 96.1 mg/L

□ pH: 10.2



# Recarbonation Model

- Addition of CO<sub>2</sub> (g)

- ▣ Lowers pH of water

- The softening process raises pH to a non-consumable level

- Input Code

- USE solution 4

- REACTION 2

- CO<sub>2</sub>(g) 1

- 0.0003 moles in 1 steps

# Recarbonation Model

## □ Phreeqc Results

### □ Hardness

■ 102.3 mg/L

### □ pH

■ 9.71



# Conclusions



- Phreeqcl is capable of mixing two different water sources to determine combined hardness and pH
- Phreeqcl can be used to simulate water softening through lime and soda ash
  - ▣ pH however is slightly lower than expected
- Phreeqcl simulates pH adjustments at a treatment plant

# Future Work/Improvements



- Ozone Disinfection
  - ▣ The addition of  $O_3$  (g) to the water
  - ▣ Formation of bromate ( $BrO_3^-$ )
- Filtration
  - ▣ pH reduction due to organics
- Removal of Organic Matter



# References

- Davis M.L., Cornwell D.A. (2008). *Introduction to Environmental Engineering*. McGraw Hill, New York.
- United States Geological Survey (1998). Frequently asked questions for PHREEQC and Phreeqc. [http://wwwbrr.cr.usgs.gov/projects/GWC\\_coupled/phreeqc/faq.html](http://wwwbrr.cr.usgs.gov/projects/GWC_coupled/phreeqc/faq.html)
- Viessman W., Hammer M.J., Perez E.M. Chadik P.A. (2009). *Water supply & pollution control*. Pearson Education Inc., New Jersey.

## Questions?